

# Debottlenecking Water-Oil Separation with Increasing Water Flow Rates in Mature Oil Fields

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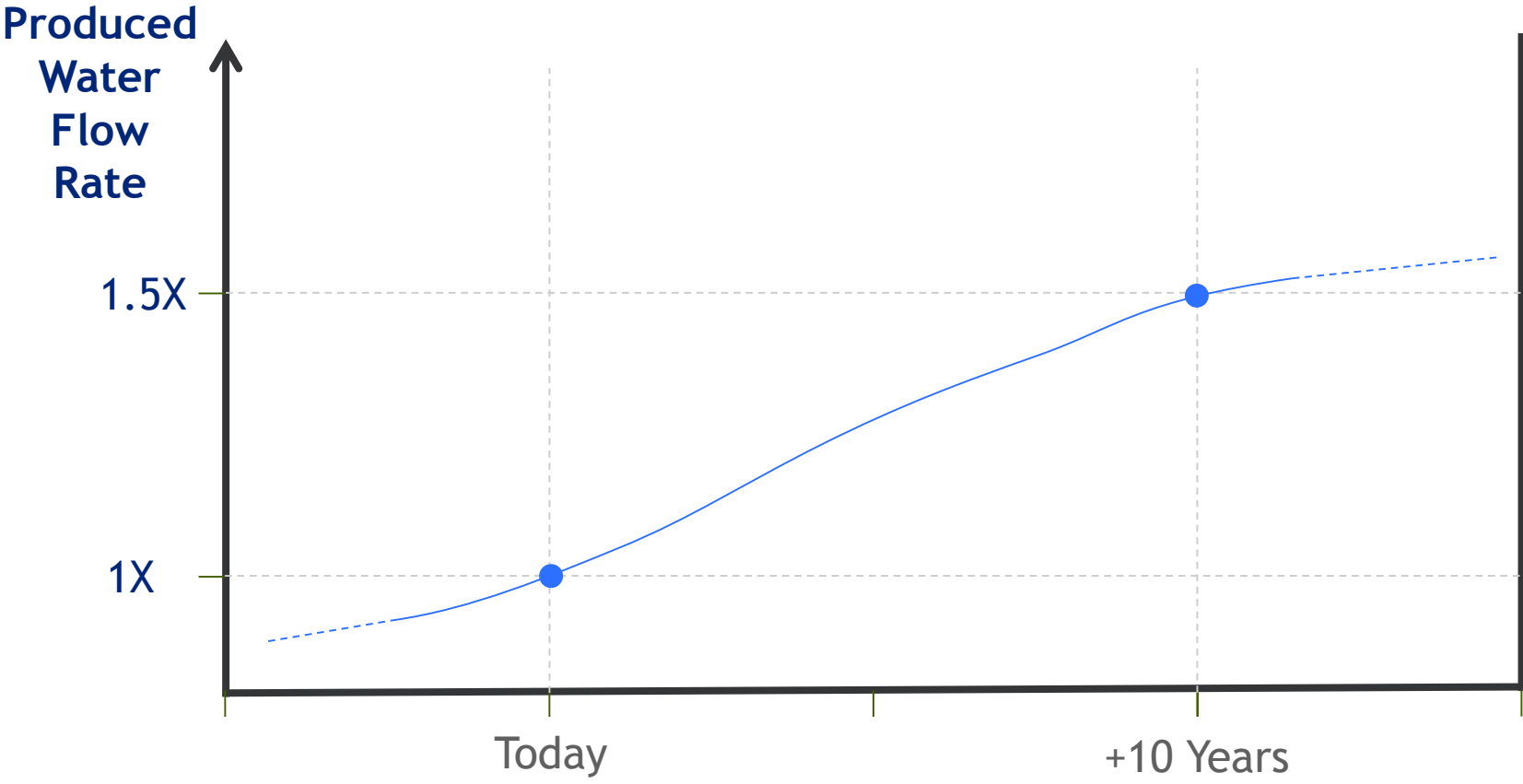
# Outline

- Background and Motivation
- Numerical Model and Test Matrix
- Results and Discussion
- Conclusions

# Background

- Maturing fields with increasing water flow rates
- For certain GOSPs, water-oil separator (WOSEP) is the bottleneck
- WOSEPs are reaching capacity to process oily produced water
- Need solution to debottleneck gas-oil separation plant for forecast rates
  - Quantify separation performance
  - Apply enhanced internal technology to improve separation at higher throughputs

# Produced Water Forecast



Not to scale

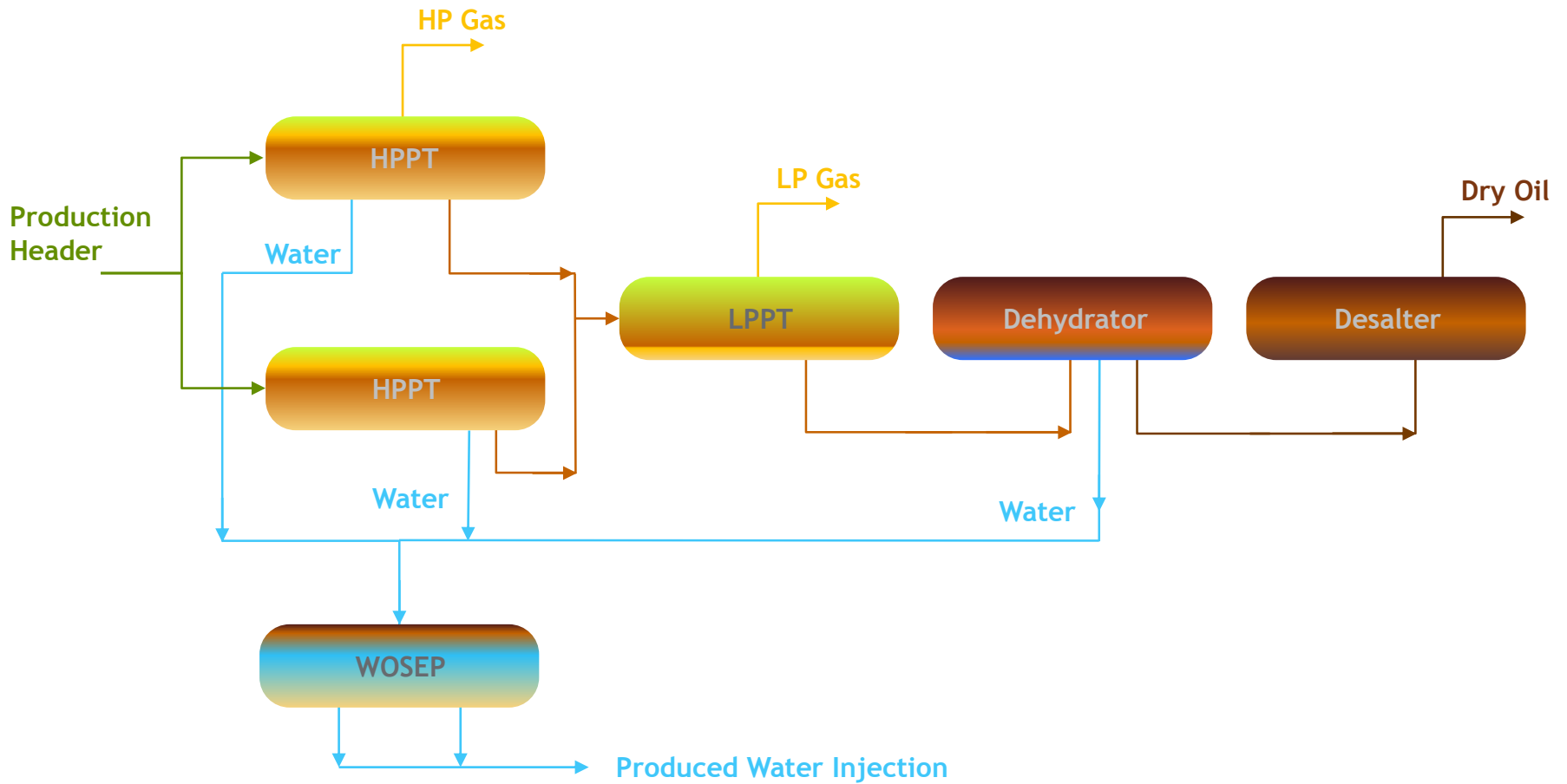
# Motivation

- Improving oil separation reduces lost production
- Improved produced water quality prevents formation damage on reinjection to maintain reservoir pressure
- Avoid the need to build additional WOSEPs in the GOSP

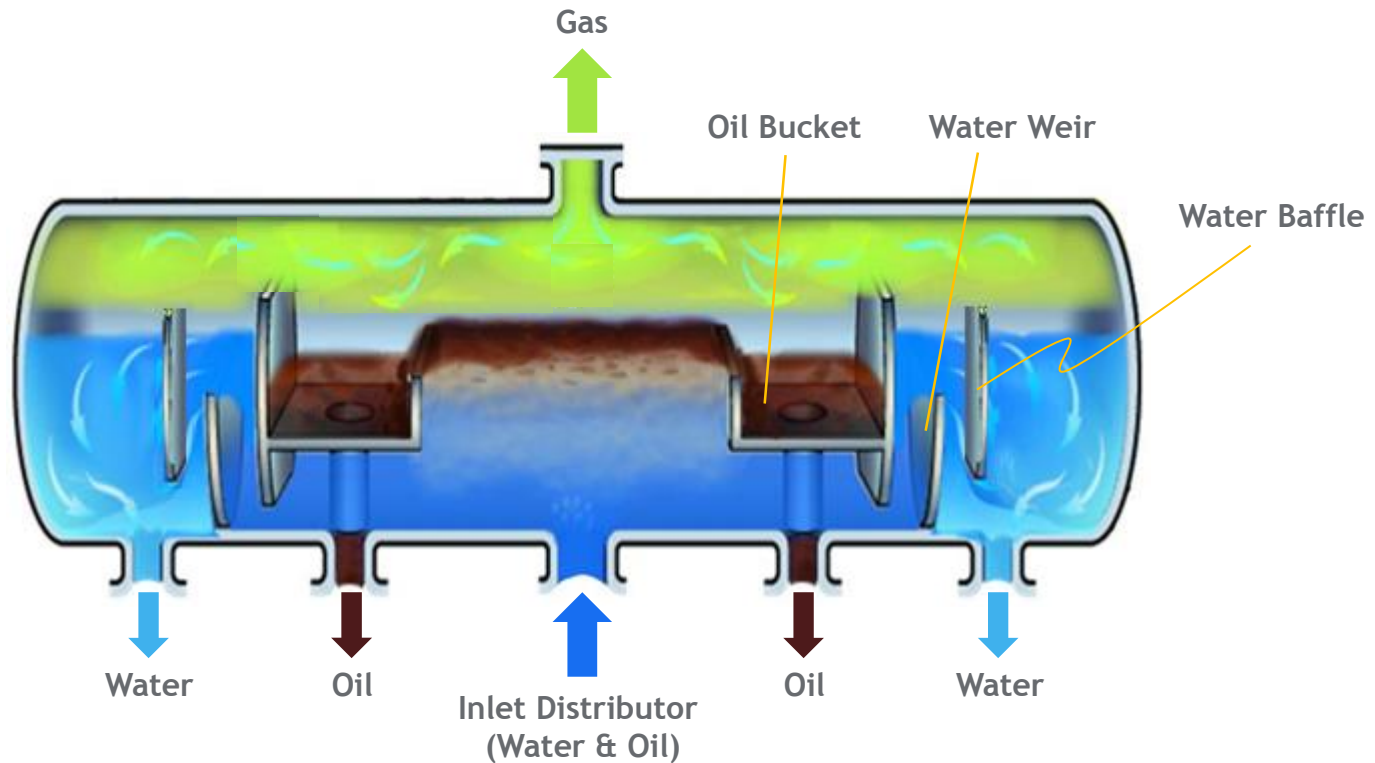
# Objectives

- Use state-of-the-art multiphase CFD to model the oil-water flow in the WOSEP vessel
- Develop debottlenecking solutions to increase water handling capacity

# Typical GOSP



# Water Oil Separation Vessel (WOSEP)

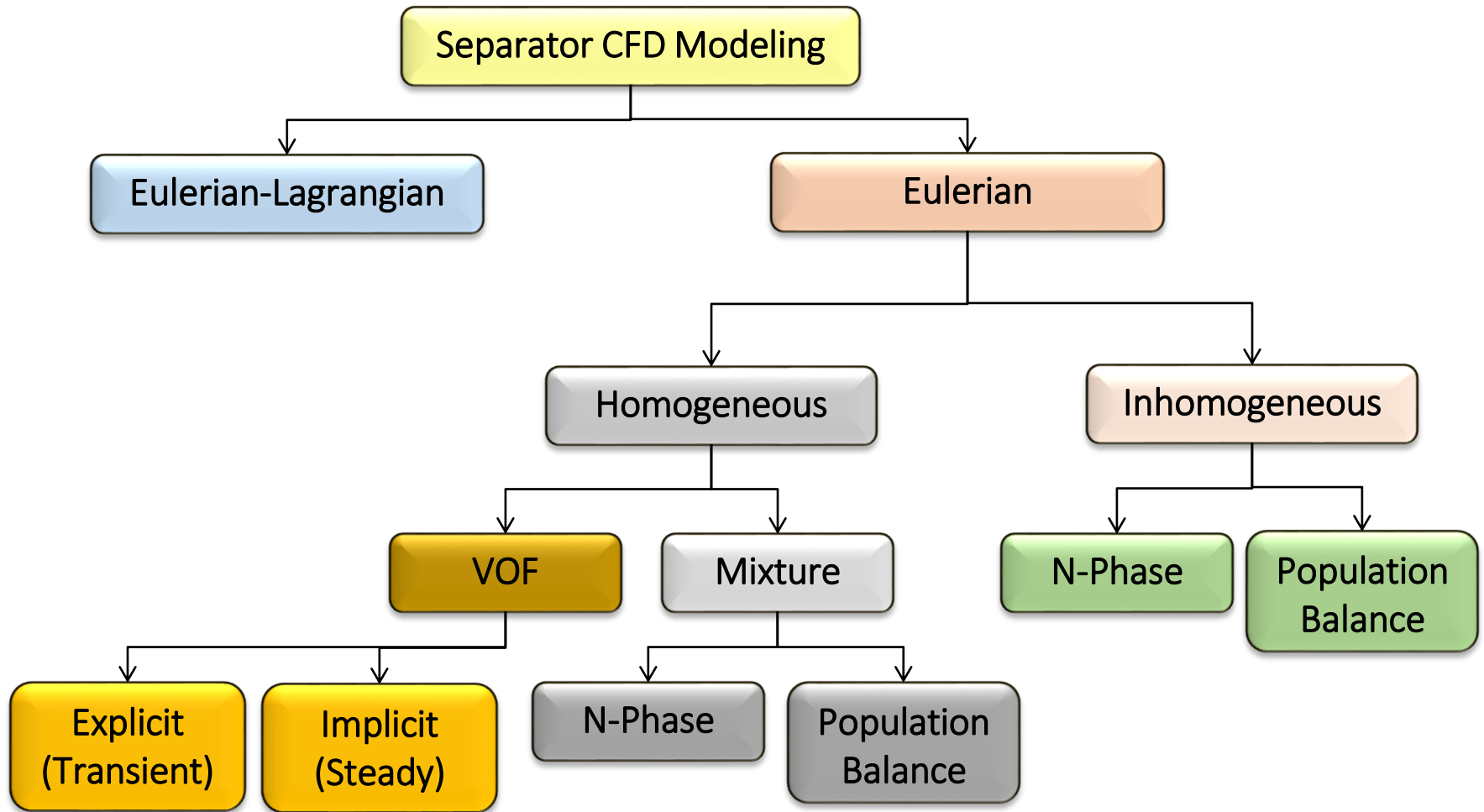


Approximate dimensions: 180 ft Length; 14 ft diameter

160 MBD Throughput



# Multiphase Modeling



# Numerical Methodology

- N-Phase Eulerian multiphase model
  - Water - primary phase
  - Oil and gas - secondary phases
- Phase interaction
  - Schiller-Naumann drag model
- Turbulence
  - Standard  $k - \varepsilon$  turbulence model with scalable wall functions
- Steady and incompressible
- High-resolution Computational mesh
  - 2 million polyhedral cells/elements

# Solution Platform

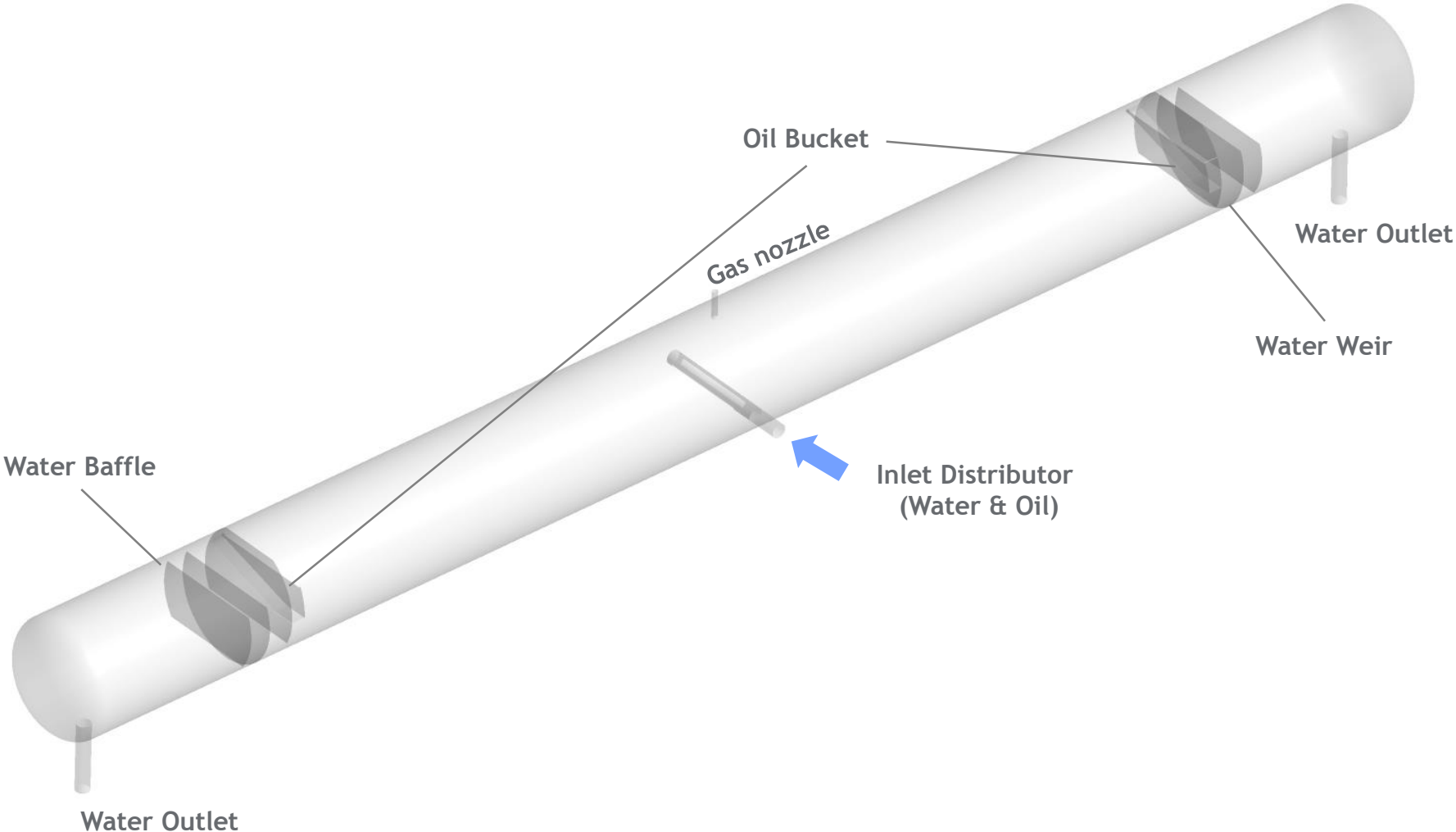
- ANSYS Workbench for Pre-Processing - Geometry and Mesh
- ANSYS Fluent R18.0 for Solution
  - Simulations run in parallel on an HPC cluster with 216 cores
- ANSYS CFD-Post 18.0 for Post-Processing

# Numerical Test Matrix

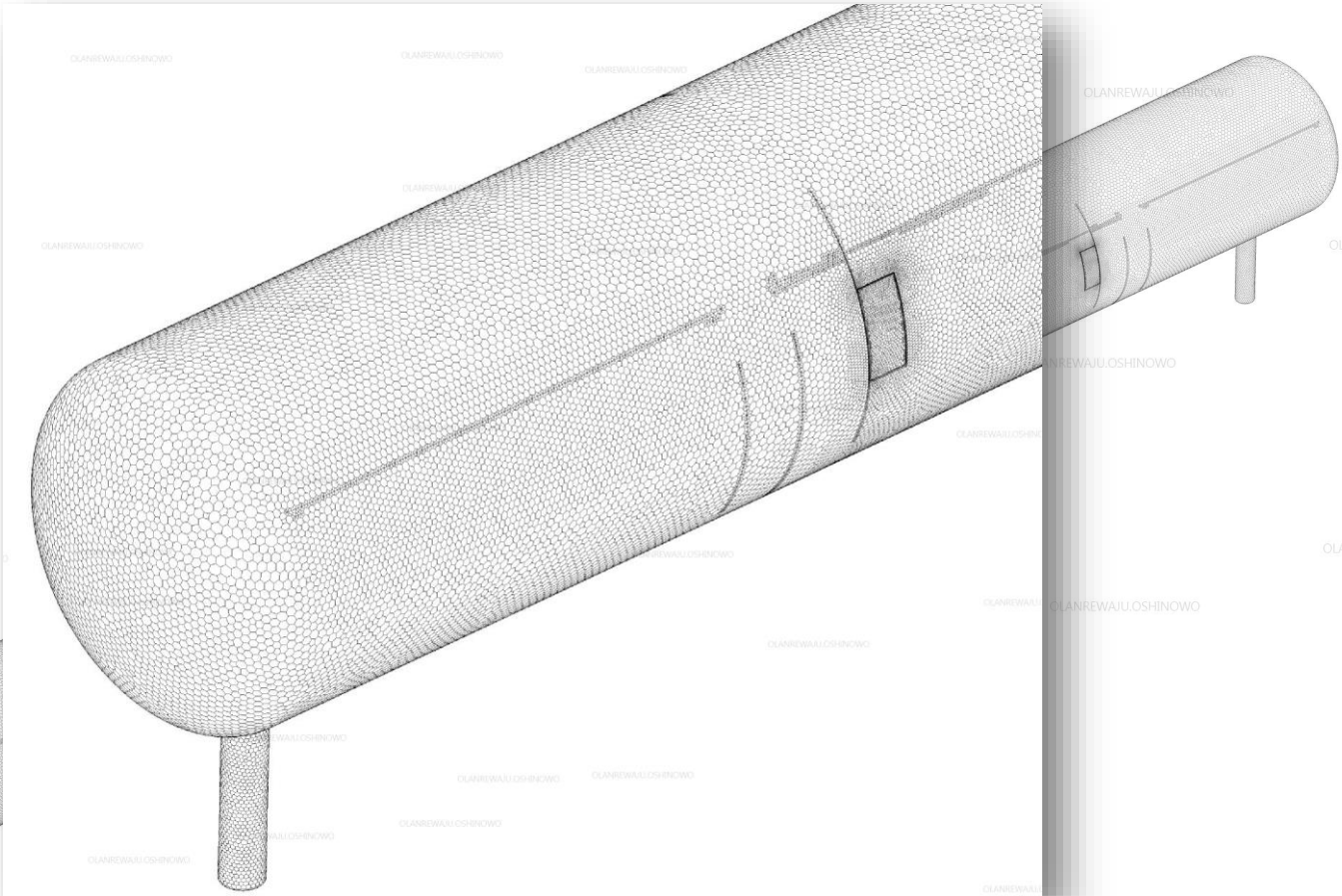
| Run | Flow (MBD) | Oil Droplet Diameter ( $\mu\text{m}$ ) |
|-----|------------|----------------------------------------|
| 1   | 173        | 10                                     |
| 2   | 173        | 50                                     |
| 3   | 265        | 10                                     |
| 4   | 265        | 50                                     |

|                         |      |
|-------------------------|------|
| Inlet Oil Fraction (OF) | 0.01 |
|-------------------------|------|

# Geometry

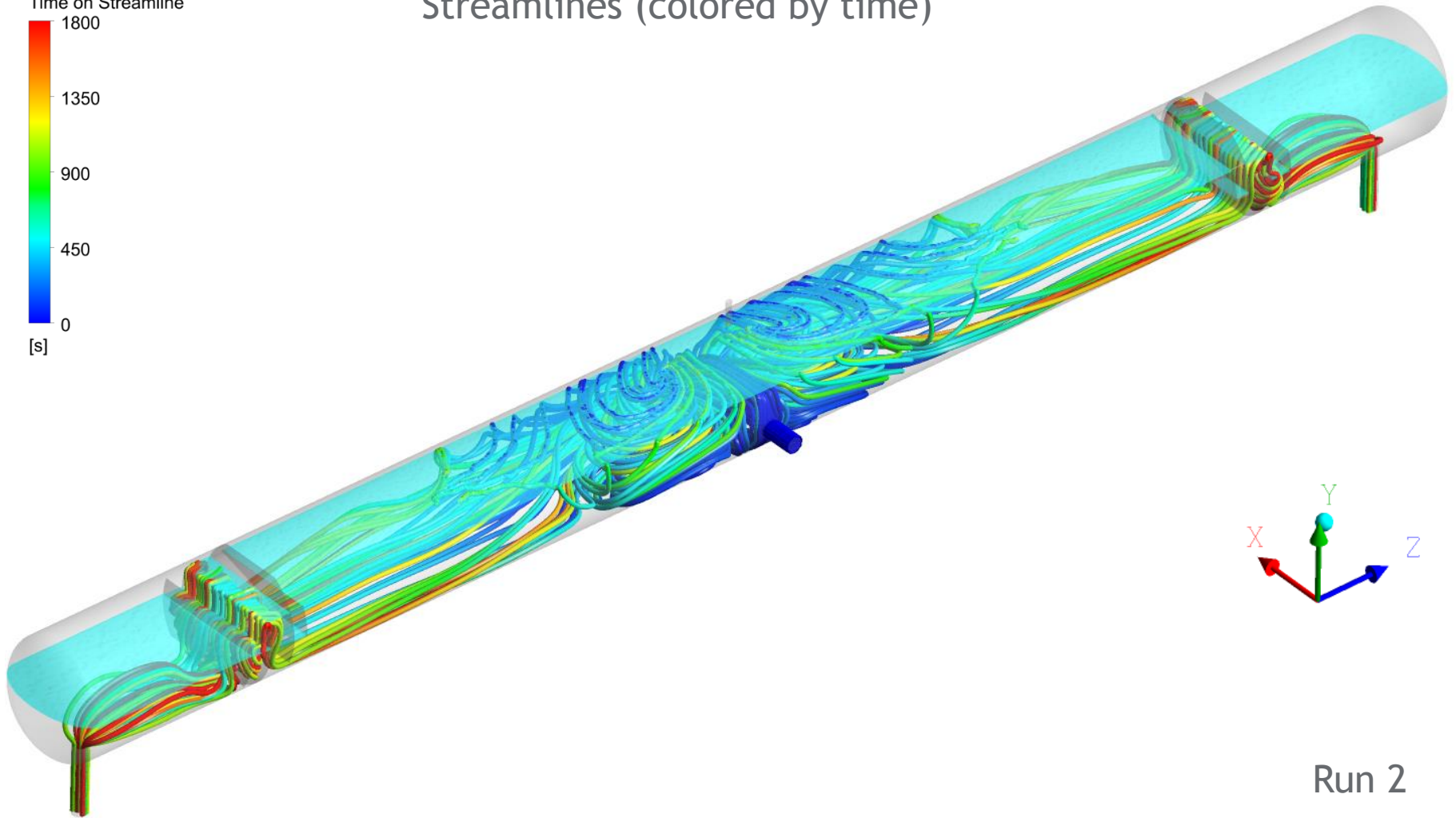
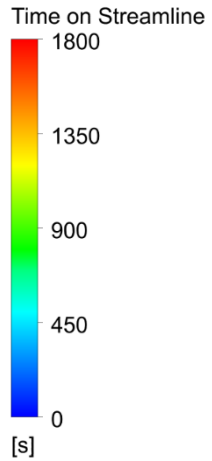


# Computational Mesh



# WOSEP Flow Field

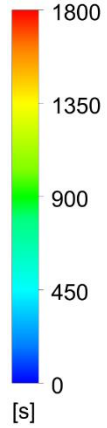
Streamlines (colored by time)



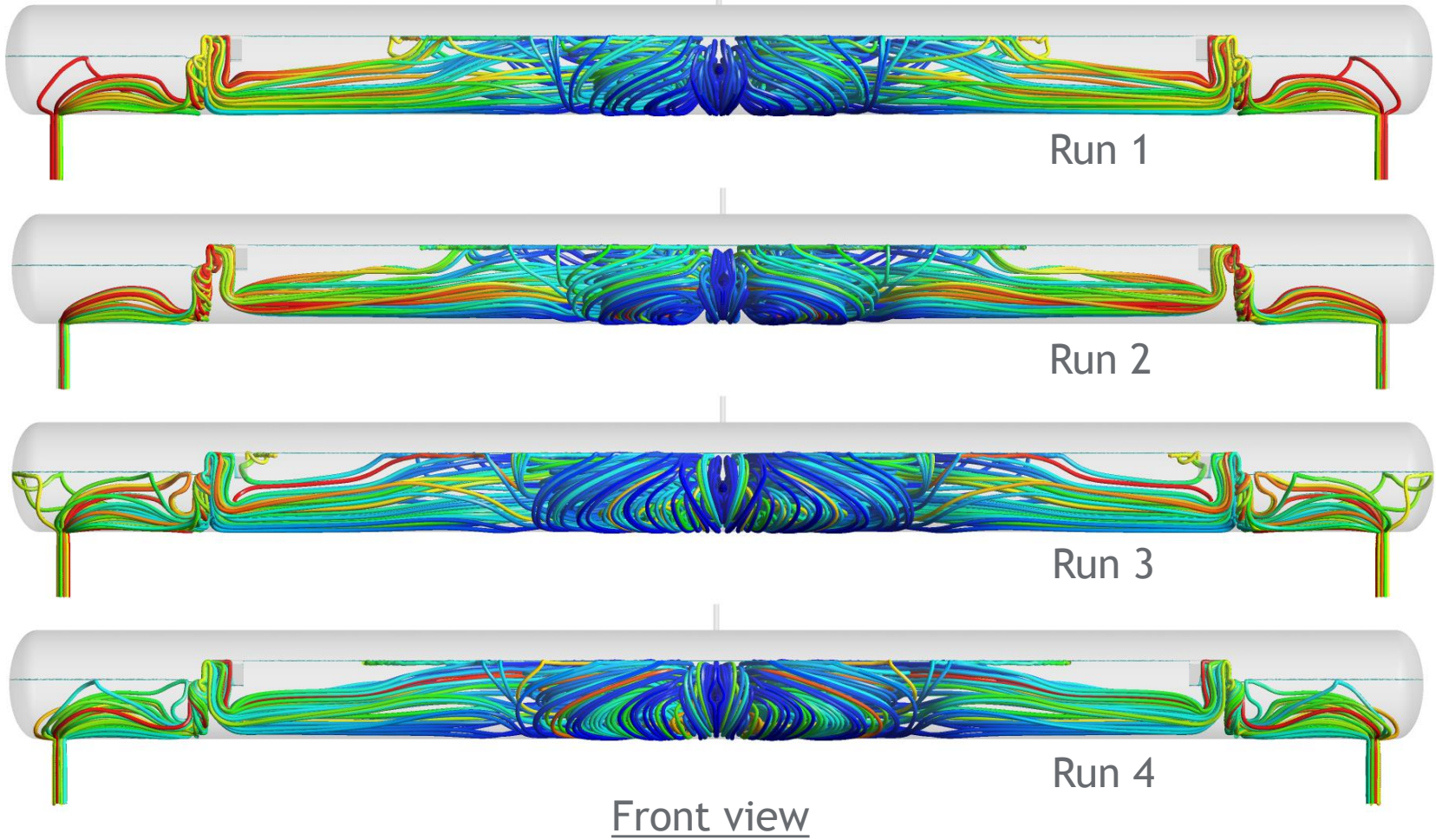
Run 2

# WOSEP Flow Field

Time on Streamline

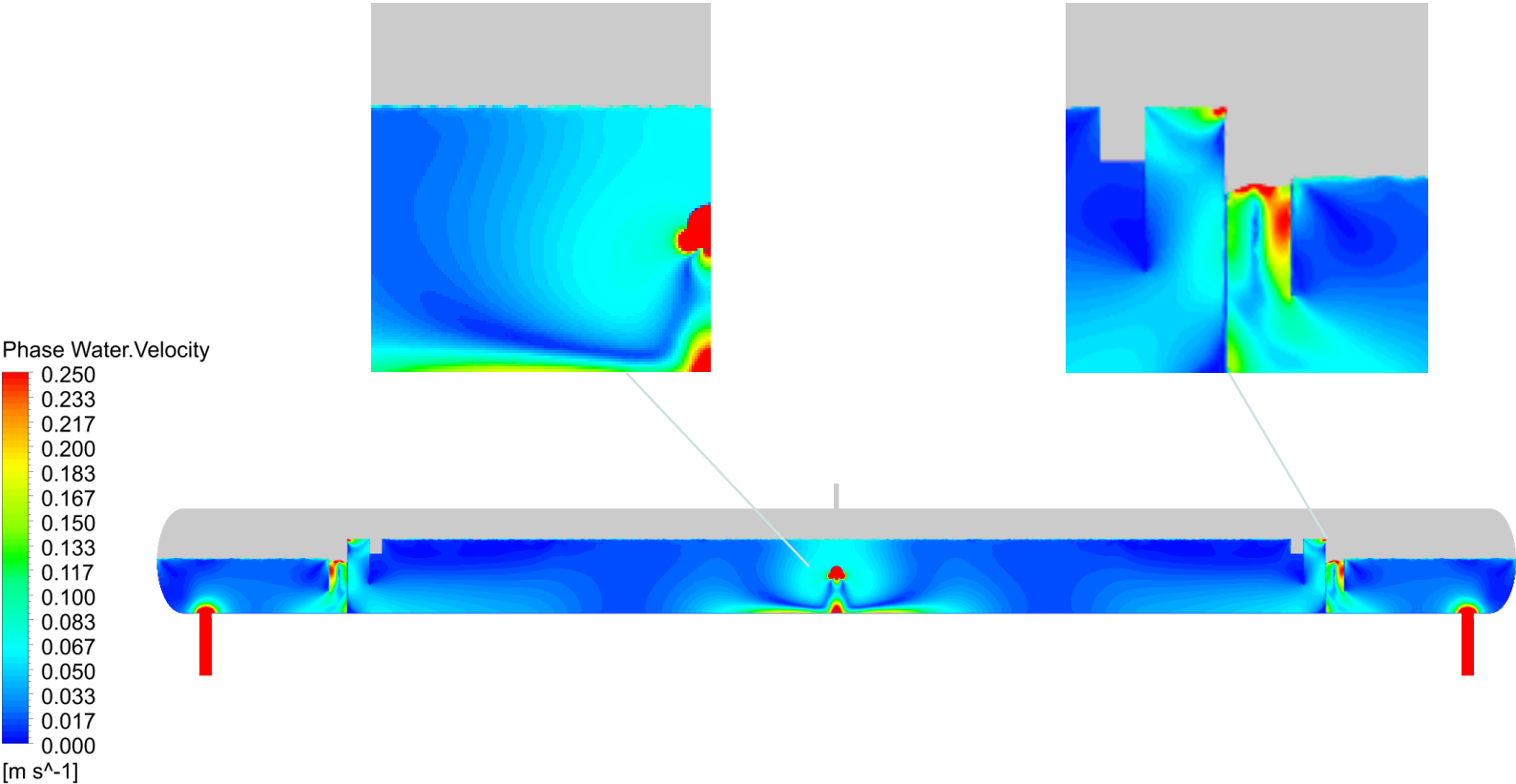


Streamlines (colored by time)



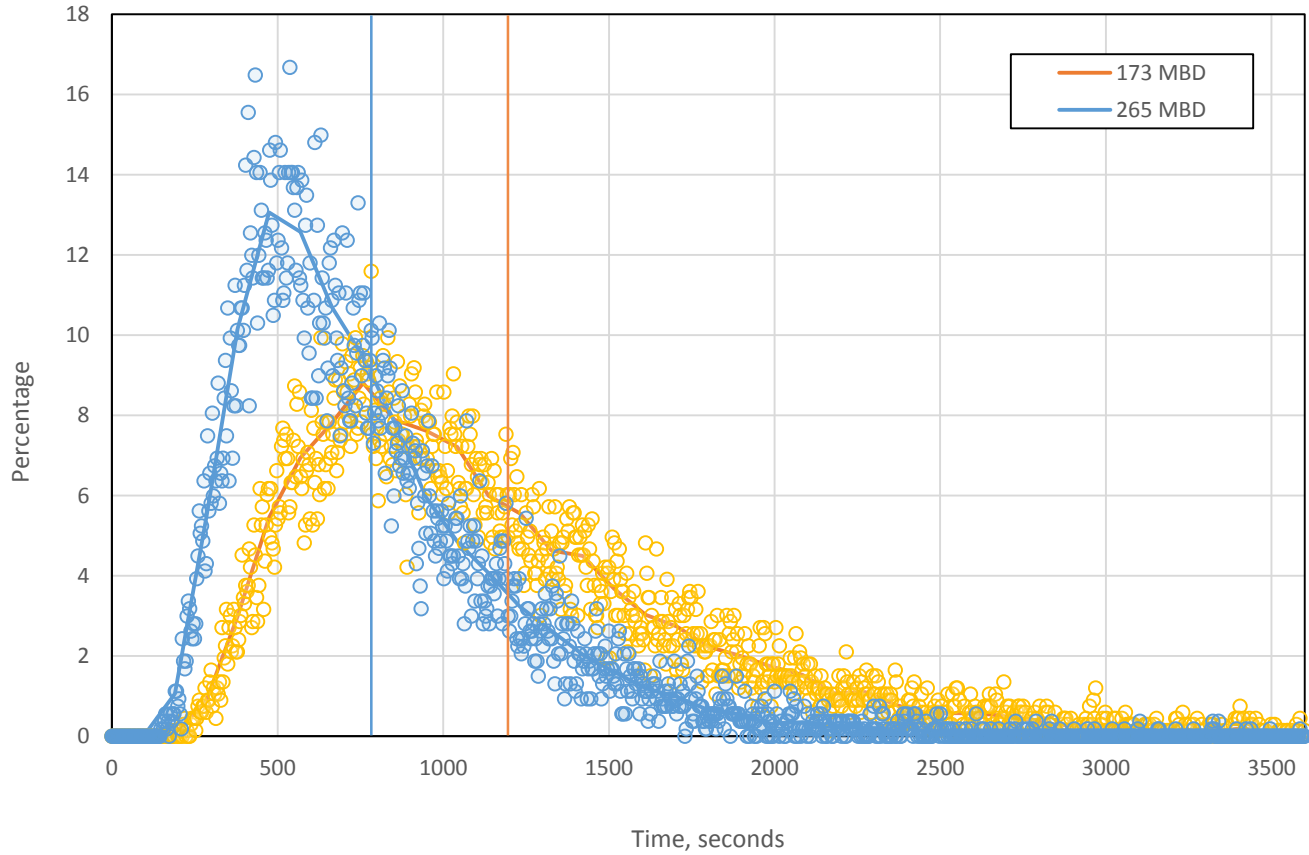


# Velocity



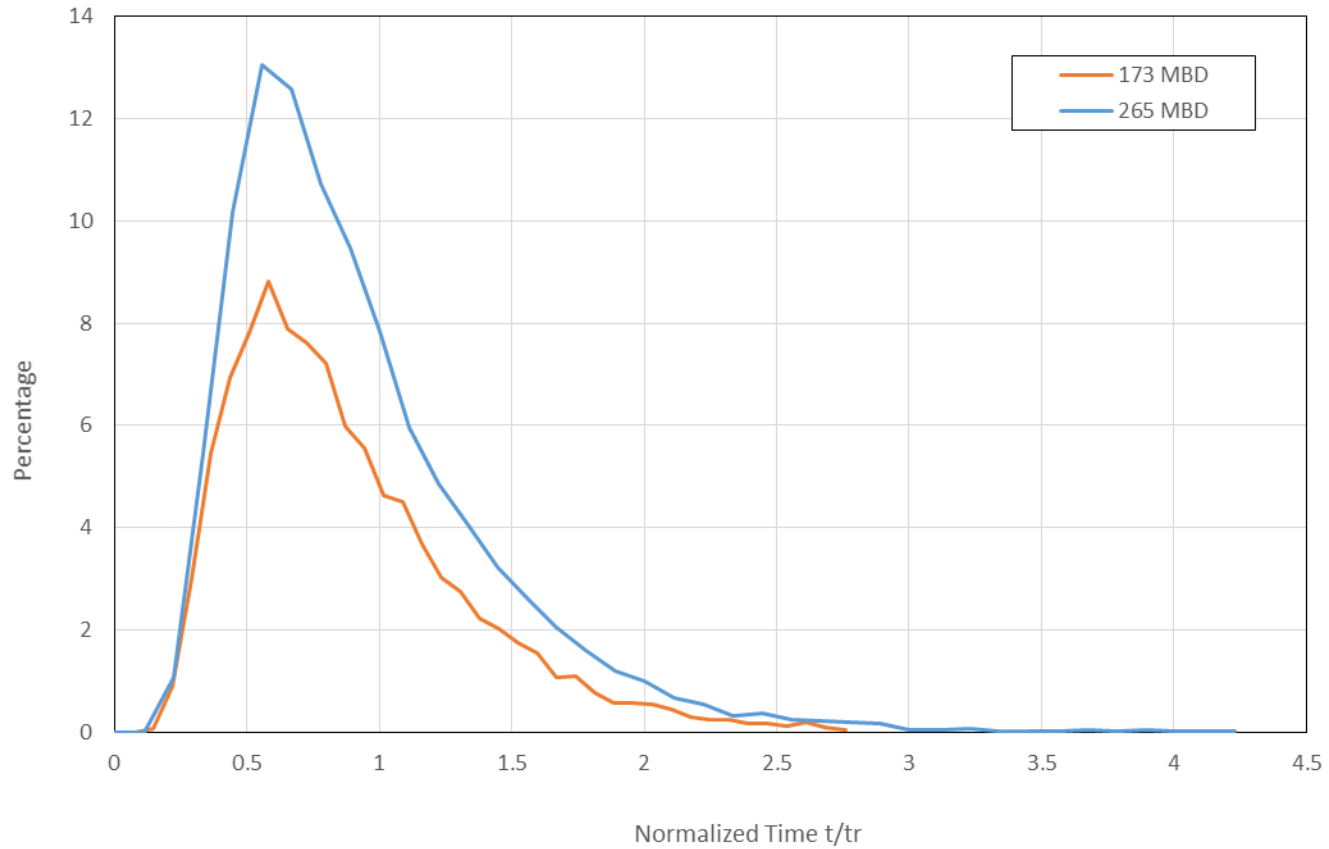
Run 2

# Residence Time Distribution

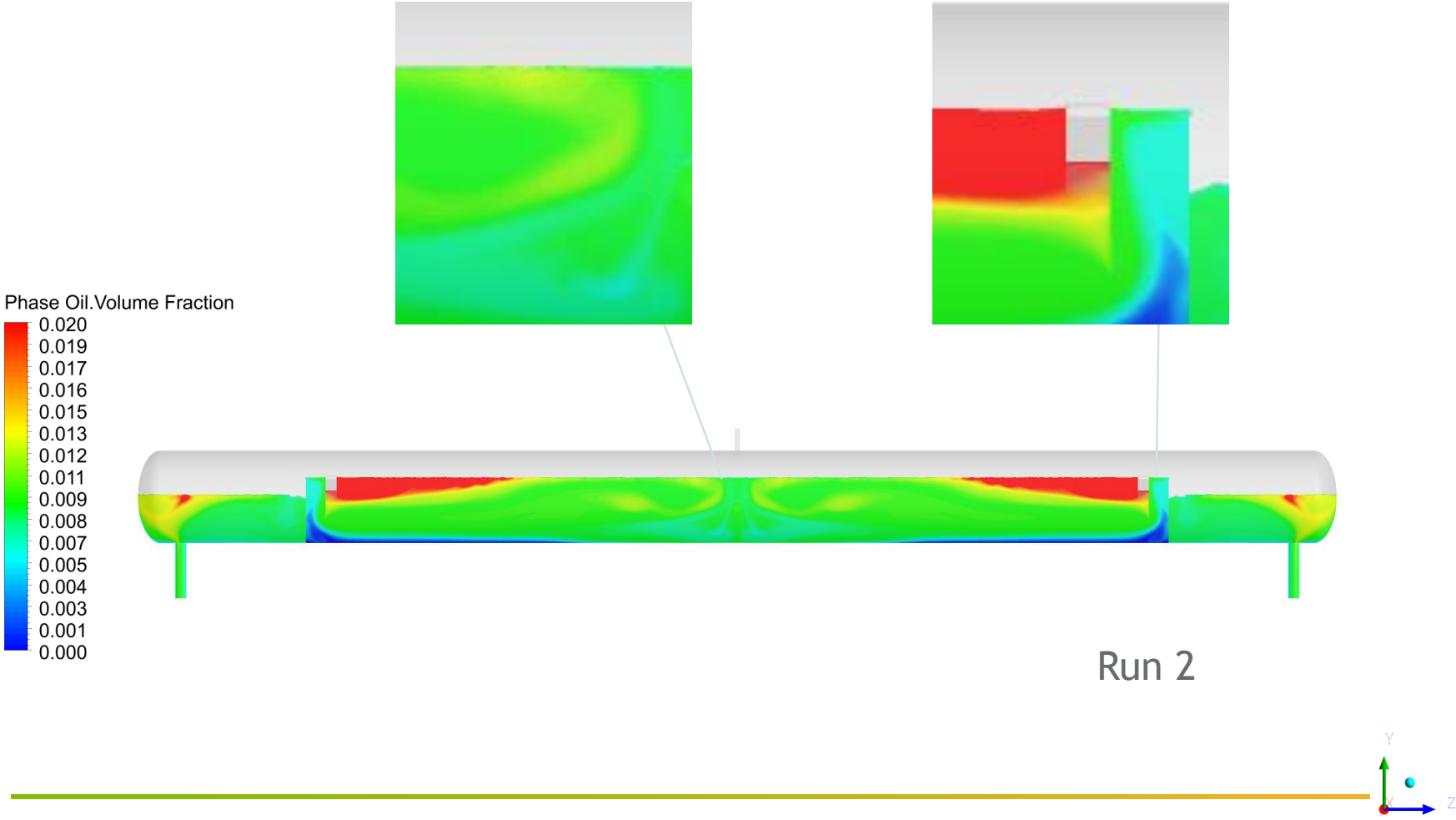


| Water Flow Rate {MBD} | Mean of RTD {s} | Retention Time ( $V_c/Q$ ) {s} |
|-----------------------|-----------------|--------------------------------|
| 173                   | 1142            | 1305                           |
| 265                   | 784             | 851                            |

# Residence Time Distribution

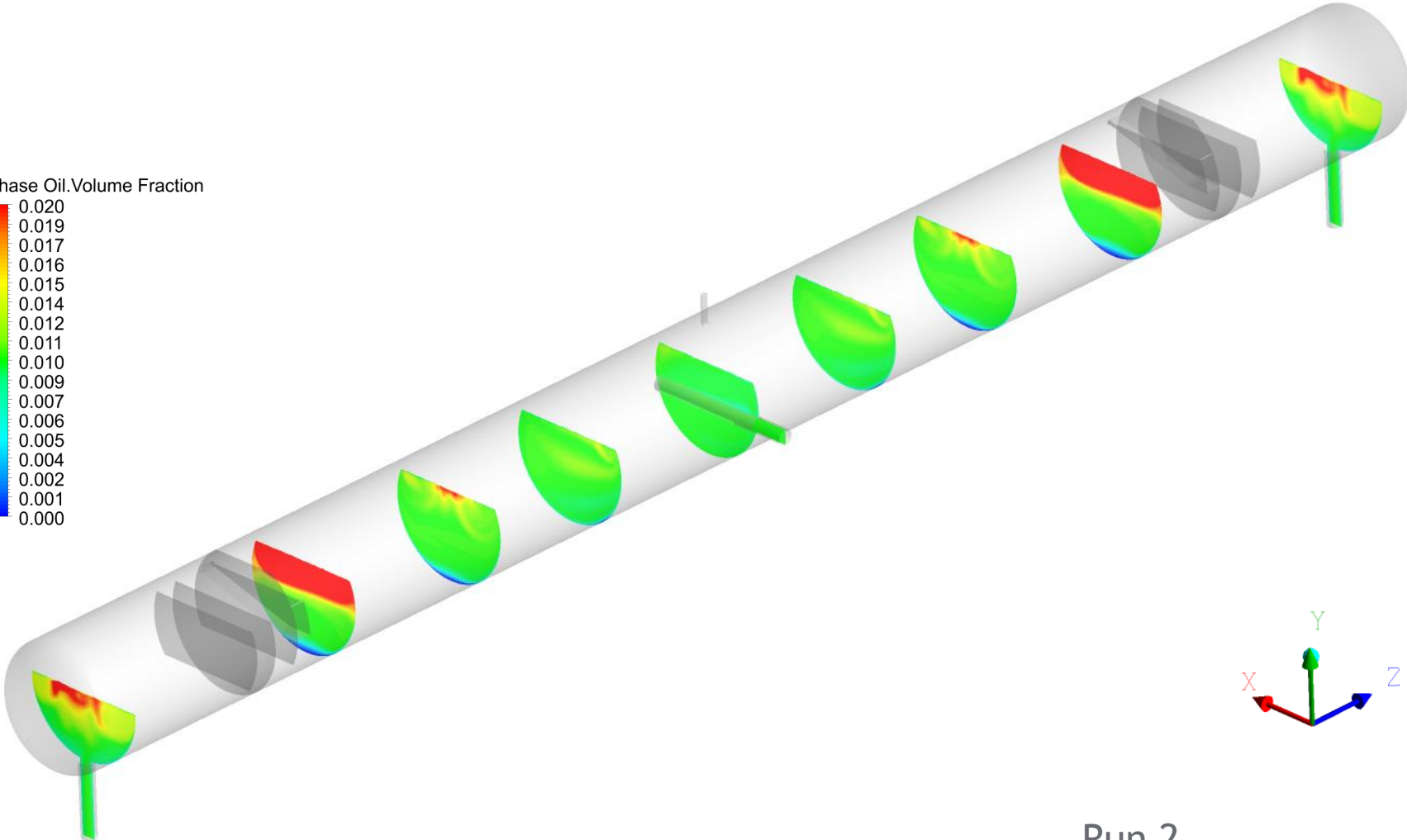
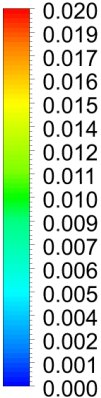


# Oil Fraction



# Oil Fraction

Phase Oil Volume Fraction



Run 2

# Effectiveness of Oil Separation

| Run | Flow (MBD) | Oil Droplet Diameter ( $\mu\text{m}$ ) | Oil Removed (%) |
|-----|------------|----------------------------------------|-----------------|
| 1   | 173        | 10                                     | <1              |
| 2   | 173        | 50                                     | 9               |
| 3   | 265        | 10                                     | <1              |
| 4   | 265        | 50                                     | 4               |

$$\text{Separation Efficiency} = \frac{\text{Inlet Oil Fraction} - \text{Outlet Oil Fraction}}{\text{Inlet Oil Fraction}} \times 100\%$$

# Conclusions

- Successful CFD simulations of WOSEP under different conditions
- Flow patterns show adverse vortices induced by the inlet distributor that reduce ability to separate oil from water
- Very low oil separation obtained from separator design for base flow rate
- Increased water throughput further reduces separation performance
- Potential to increase primary stage produced water oil removal through improvements in WOSEP design:
  - Inlet distributor
  - Additional internals (perforated plate baffles or derivatives, coalescing plate packing)
  - Vessel configuration

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