



A Bench Scale Study: Demonstrating Chloramine Disinfection Potential Using Liquid Ammonium Sulfate

Lamees Alkhamis,
P.E., MSc
Civil & Environmental Engineer
lamees.alkhamis@stantec.com

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Agenda

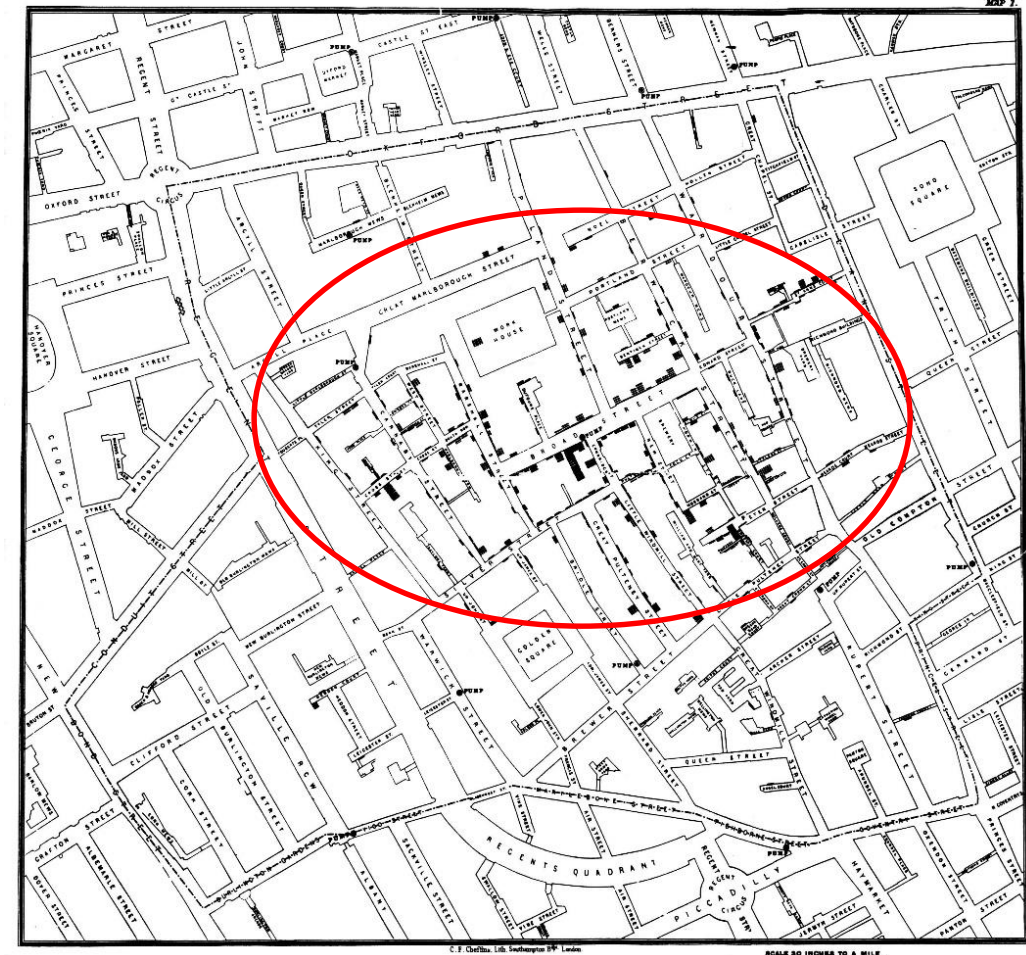
1. Introduction to Chloramination
2. Bench Scale Study Introduction
3. Bench Scale Study Calculations and Procedures
4. Bench Scale Study Results and Conclusions

1. Introduction to Chloramination

Disinfection

1 Introduction to Chloramination

- Drinking water disinfection using chlorination began in Mid 1800's to reduce waterborne diseases
- Chlorination is the most used disinfectant in GCC countries and worldwide



John Snow's Cholera Outbreak Map of Soho London

Chlorine Chemistry

- Chlorine is used as a disinfectant either by gas or liquid form:

Chlorine Gas (Cl₂) *poisonous if released in the air*



Sodium Hypochlorite (NaOCl)

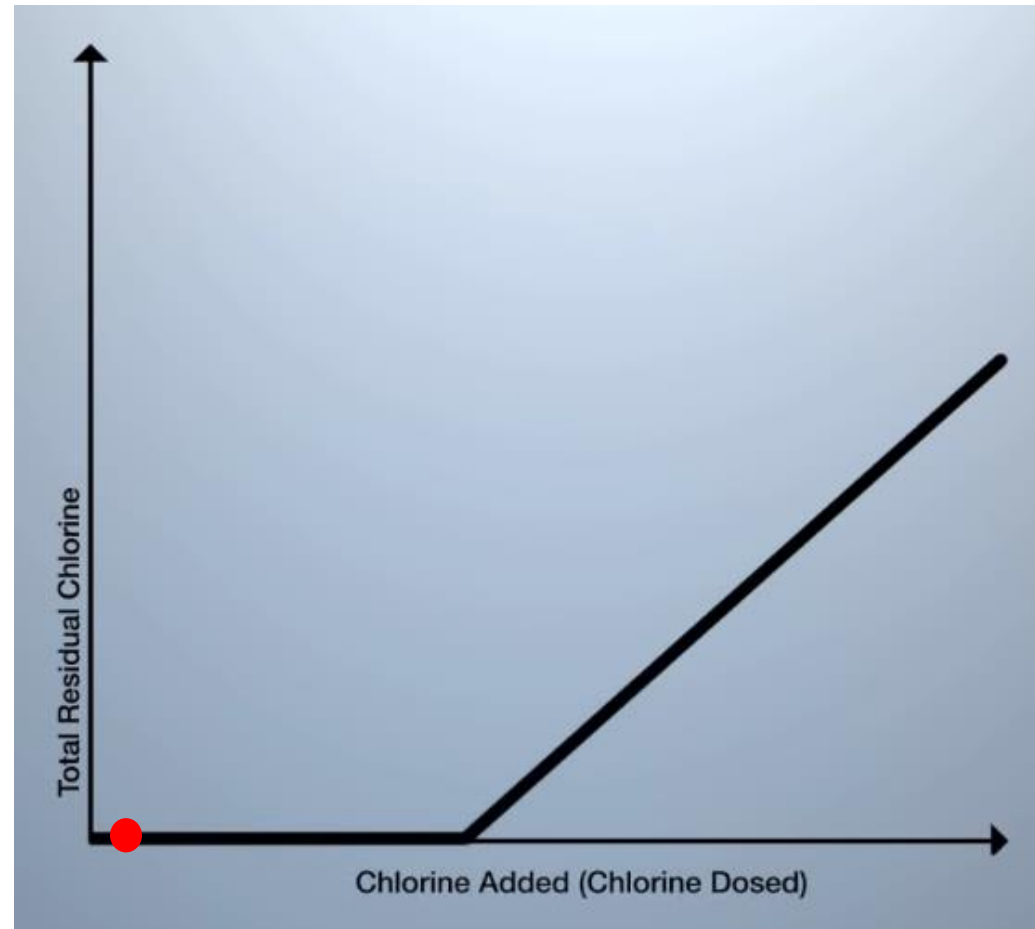


- The two species formed by chlorine in water is hypochlorous acid (HOCl: above pH 7.5) and hypochlorite ion (OCl⁻ below pH 7.5)



Chlorine “Breakpoint” Curve

- Chlorination curve describes what happens when chlorine added to water



Source: HACH

Chloramination Definition and Forms

- Chloramination is an alternative disinfection method, where a small quantity of ammonia is added to chlorinated water
- Chloramines are formed when free chlorine reacts with free ammonia present in the water forming:
 - Monochloramine (NH_2Cl) **desired form**
 - Dichloramine (NHCl_2)
 - Trichloramine (NCl_3)

Note:

- Monochloramine has high concentration and time (CT) value thus poor primary disinfectant
- However, high CT makes it ideal as a secondary disinfection in the distribution system

Chlorination Disadvantages and Advantages

- Chlorination Disadvantages:

1-Chlorination has the potential to react with natural organic matter and form chlorinated disinfectant by-products (DBPs) for **surface water sources**

- θ DBPs have been shown to increase the risk of bladder cancer, among other health consequences
- θ Main DBP's include:
 - Total trihalomethanes (TTHMs)
 - Haloacetic acids (HAA5)
 - Nitrosamines: N-Nitroso-dimethylamine (NDMA)

Chlorination Disadvantages and Advantages

- Chlorination Advantages:

1-It is recognized that chlorination will continue to be the most common disinfection process

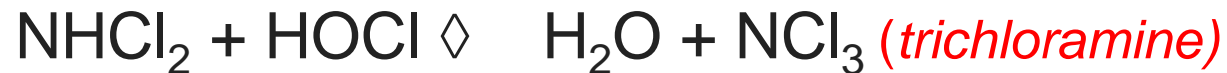
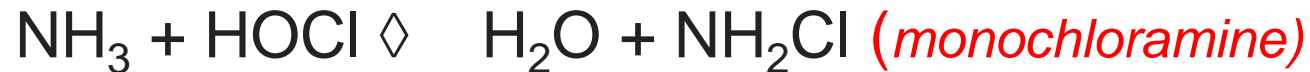
θ Enhanced removal of DBP precursors from raw water sources can be done by GAC and nanofiltration

Chloramination Disadvantages and Advantages

- Chloramination disadvantages:
 - 1- It is a poor oxidant and
 - 2- It is not effective for taste and odor control or for oxidation of iron and manganese
- Chloramination advantages:
 - 1- Eliminate the formation of chlorination by-products,
 - 2- Maintains long residual
 - 3- More economical than alternative disinfection methods (e.g. Ozone and UV disinfection)

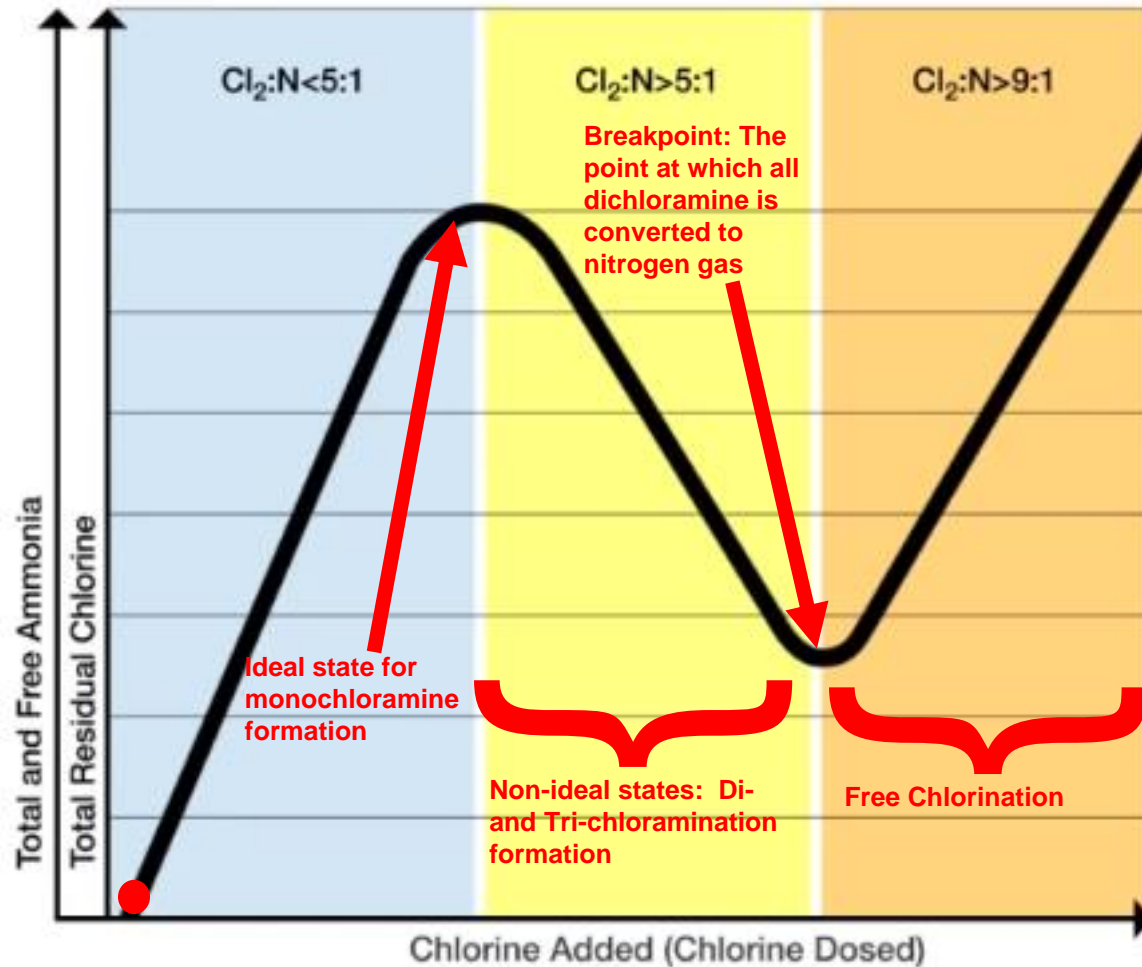
Chloramination Chemistry

- WTPs use chloramine compounds in the form of aqueous ammonia (**NH₄OH, AA**) and sodium hypochlorite (**NaOCl, SH**).
- Chloramines are frequently produced by adding ammonia to water containing free chlorine (ideal pH 8.4)



Chloramination Curve

- Chloramination curve describes what happens when chlorine added with ammonia in water



Source: HACH

2. Bench Scale Study Introduction

The Client “EBMUD” Drivers for the Study

- EBMUD has a CSSIP to improve safety of all chemical process in WTP
- The use of AA has an **inherent risk** of ammonia vapor exposure to operators and to the general public in the vicinity
- Liquid ammonium sulfate ($(\text{NH}_4)_2\text{SO}_4$, **LAS**) is identified as a chemical substitute to AA
- Continued use of AA for chloramination will require several major safety and code upgrades at the client’s WTPs
- Substitution of LAS for AA, reduces several safety, code, reporting, maintenance requirements and maintenance cost



**AQUEOUS
AMMONIA**

Chemical Properties: AA versus LAS

Property	Aqueous Ammonia (Ammonium Hydroxide), AA	Liquid Ammonium Sulfate, LAS
Formula	$\text{NH}_4(\text{OH})$	$(\text{NH}_4)_2\text{SO}_4$
Concentration	19-20%	38-40%
Density	992.7 g/L	1,222.2 g/L
Available Ammonia	185.7 g NH_3 / L AA solution	121 g NH_3 / L LAS solution
pH	11.6	3.0-5.0
Volatility	High vapor pressure (32.5 kPa @ 21 C) Off-gassing of ammonia vapors	Non-volatile, stable, does not off-gas (1.8 kPa)
Odor	Strong	No odor

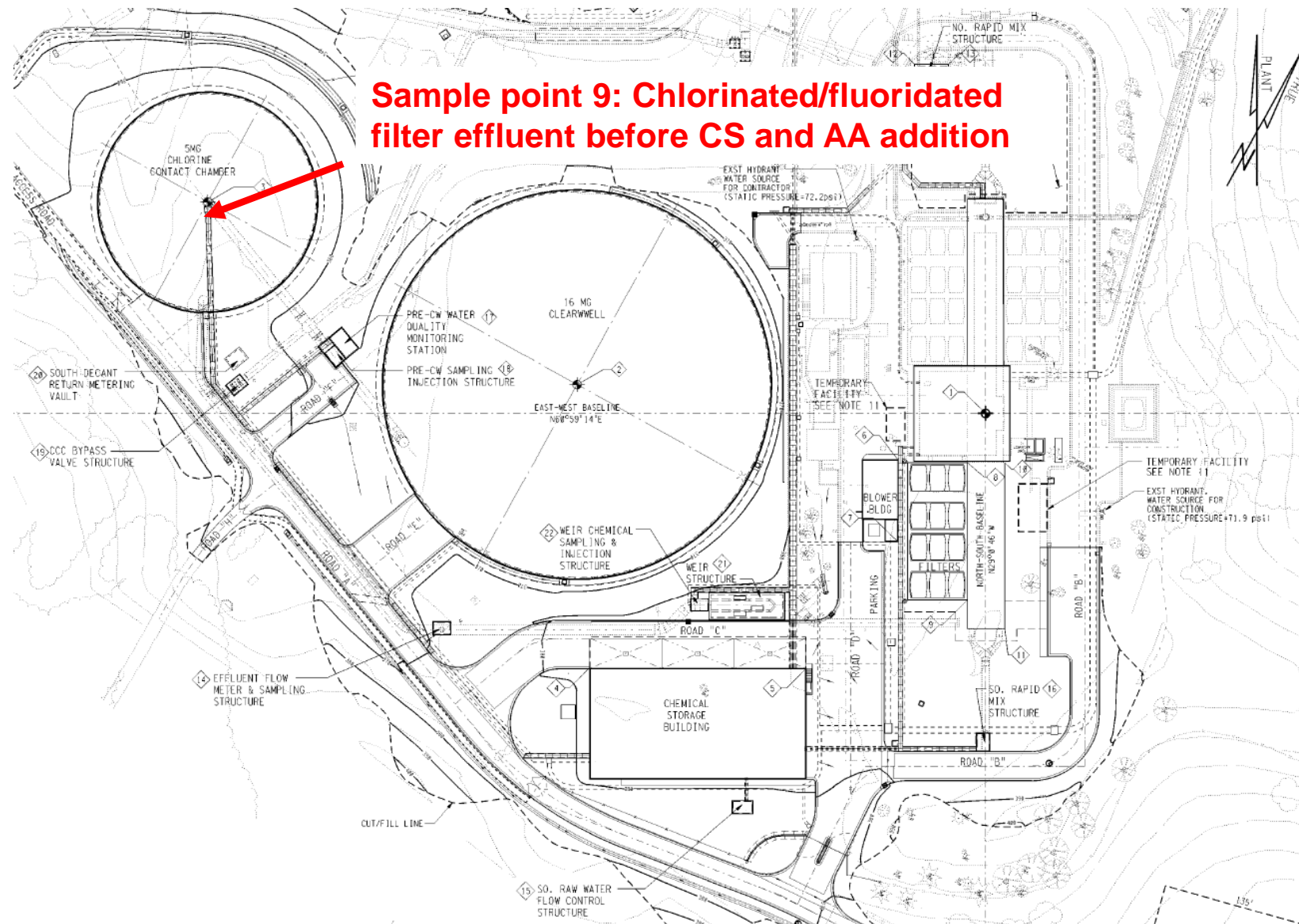
Walnut Creek WTP in California, USA

- Walnut Creek WTP has a treatment capacity of 115 MGD (435,322.4 m³/d)
- The water source is Pardee Reservoir in the Sierra
- The treatment process utilizes direct filtration – skips flocculation phase and coagulation occurs in-line prior to rapid mix



Walnut Creek WTP Process

2 Bench Scale
Study
Introduction



Sample point 9: Chlorinated/fluoridated filter effluent before CS and AA addition

Objectives of the Bench Scale Study

1. Determine and verify the dose of SH to LAS and caustic soda (CS) to LAS, in order to:
 - (a) achieve a chlorine to ammonia ratio ($\text{Cl}_2:\text{N}$) of at **least 4.7** but not **exceeding 4.9** which is the optimal ratio for monochloramine formation
 - (b) increase the **pH** of the effluent treated water to **9.2** for corrosion control in the distribution system

Objectives of the Bench Scale Study

2. Compare DBP formation for AA/SH and LAS/SH to the maximum contaminant level (MCL) allowed
3. Compare the rate of chloramine decay when using AA/SH vs. LAS/SH to ensure a lasting chloramine residual is maintained

3. Bench Scale Study Calculations and Procedures

AA, LAS and CS Concentrations

- Below summarizes stock solution concentrations used and calculated

Chemical	Units	AA		LAS	CS
Formula	--	NH ₄ OH	NH ₃	(NH ₄) ₂ SO ₄	NaOH
Molecular Weight	g/mol	35.04	17.031	132.14	40.1
% of Product	--		19%	40%	50%
Specific Gravity/Relative Density	--	0.9		1.23	1.53
Stock Concentration	mg/L		170,684	491,090	761,090
Stock Concentration – N	mg/L		140,307	104,060	N/A
Dilution (mL Stock to mL Water)	--		100	100	1000
Diluted Concentration	mg/L		1,403.07	1,040.60	761.09
	mg/mL		1.40	1.04	0.76

NH₄-N Dose Calculation

- The testing does of ammonia in the form of AA and LAS is determined from the free-chlorine concentration measured in the tested water to satisfy the (Cl₂:N) ratio desired

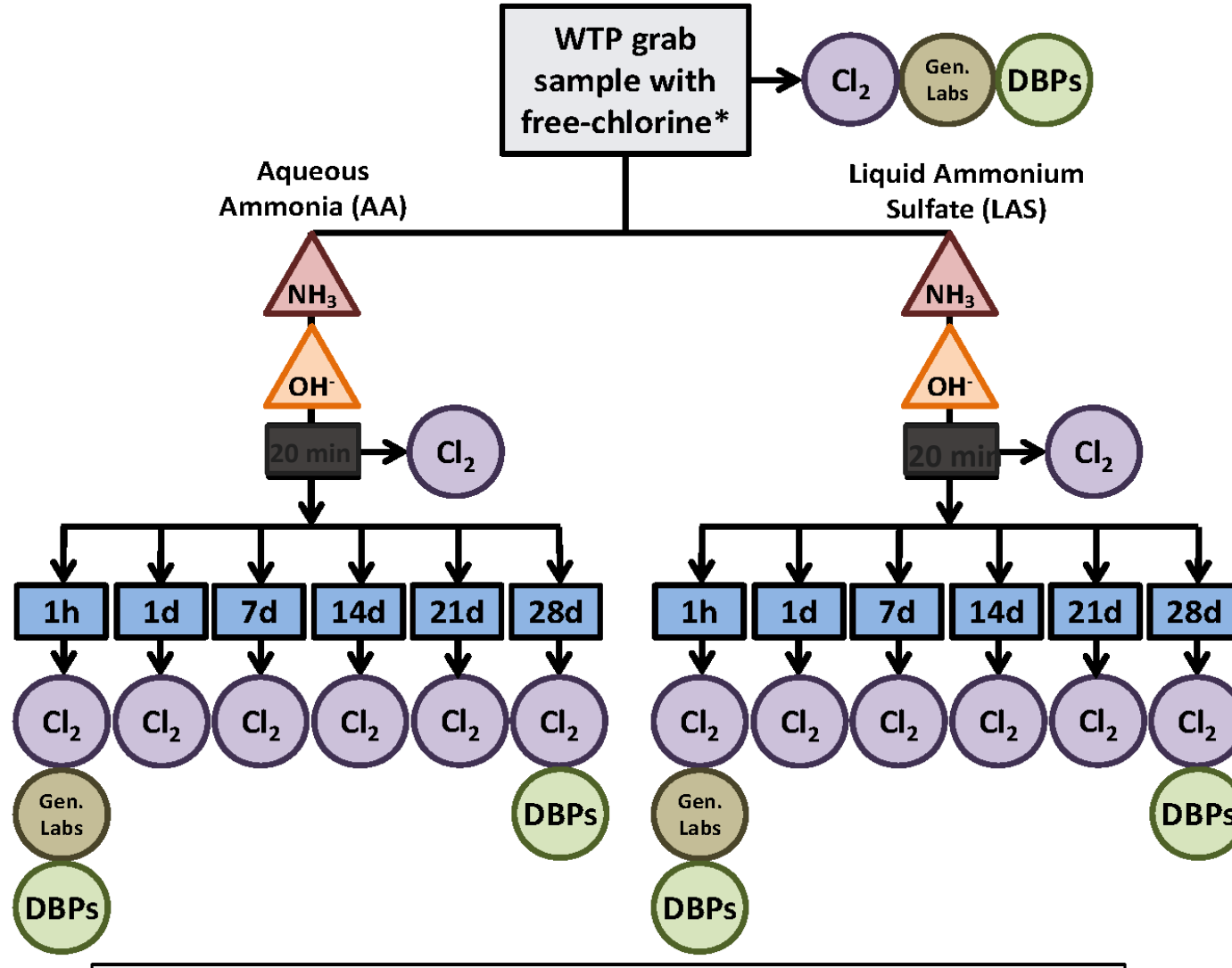
- Example of NH₄-N dose calculation:

Free chlorine residual (mg/L)	2.61	← Measured from sample point
Time of measurement	9:08	
Desired ratio (Cl ₂ :NH ₄ -N)	4.8	
NH ₄ -N dose (mg/L)	0.544	← Calculated from ratio desired

- LAS and AA are calculated according to the NH₄-N dose in the red box

Testing Procedures

3 Bench Scale
Study
Calculations and
Procedures



Legend

	Perform analysis at WTP Lab: pH, temperature, total chlorine, monochloramine, free ammonia, turbidity
	Collect sample for lab analysis for alkalinity, conductivity, TDS, calcium, anions (Cl, SO ₄ , NO ₂ , NO ₃), TOC, TKN.
	Collect sample for lab analysis for TTHMs, HAA5, and nitrosamines
	Dose ammonia (either AA or LAS) to reach a Cl ₂ :NH ₃ between 4.7-4.9. Mix well.
	Adjust final with caustic to pH: <ul style="list-style-type: none"> • 9.2 for inline filter plants • 8.5 for conventional plants
	Total hold time after ammonia addition in minutes (m), hours (h), or days (d)

Testing Procedures – Dose Determination and Data Sheet

- A sample dose determination for AA and data sheet while testing is shown below:

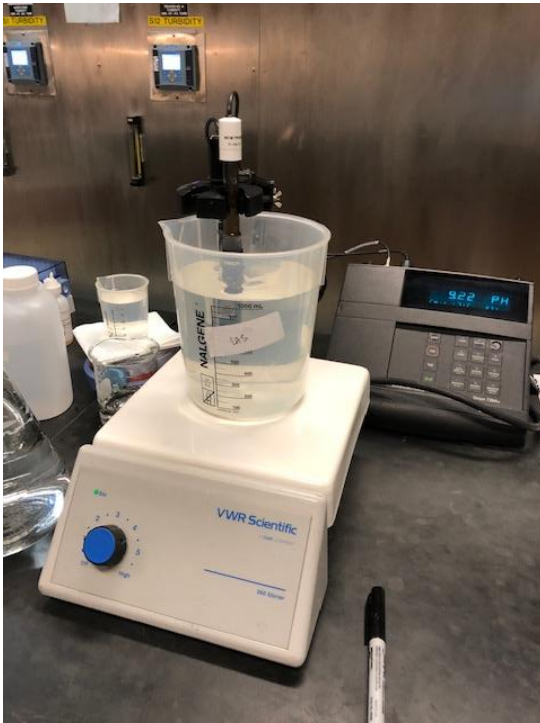
LAS/AA + CS Dose Determination			
Working volume (L)	1	1	1
Chemical	AA	LAS	CS (AA)
diluted stock concentration - N mg/mL	1.40	1.04	0.76
volume to add per L mL/L	0.39	0.52	
volume to add per 1L of sample (mL)	0.39	0.52	3.94
concentration (mg/L)	0.544	0.544	< to be determined by titration

AA + CS Titrations	Trial 1			Trial 2		
	mL AA added	mL CS added	pH	mL AA added	mL CS added	pH
	0.39	0	8.37	0.39	0	8.34
		1	8.77		3.3	9.22
		1	9		0.2	9.23
		0.5	9.08			
		0.2	9.11			
		0.2	9.14			
		0.2	9.17			
		0.2	9.2			
		3.3	9.2		3.5	9.23
AA concentration (mg/L)	0.544			0.544		
actual CS concentration (mg/L)	2.50			2.65		

AA and LAS
Concentration
Determination
(Cl₂:N)

CS Concentration
Determination (pH)

Testing Procedures – Photos



CS concentration
determination of LAS sample



Spigots containing LAS/CS
and AA/CS samples prior to
lab analysis



Outside lab analysis samples

4. Bench Scale Study Results and Conclusions

Test Results

- **Objective 1:** (a) achieve a **Cl₂:N** of at least **4.7 but not exceeding 4.9**
- (b) **pH** of the effluent treated water to **9.2**. Achieved based on Data below

AA+CS	0m	20m	1h	1d	7d	14d	21d	28d
Date	4/11/2018	4/11/2018	4/11/2018	4/12/2018	4/18/2018	4/25/2018	5/2/2018	5/9/2018
Time	15:05	15:25	16:05	15:17	11:01	15:02	8:22	8:34
Location	WCWTP	WCWTP	WCWTP	PP	PP	PP	PP	PP
pH		9.23	9.25	9.34	9.26	9.24	9.21	9.24
Temperature (deg C)		16.5	16.8	14.9	14.4	14.8	15.2	15.2
Total Chlorine (mg/L)		2.63	2.6	2.48	2.33	2.2	2.14	2.08
Monochloramine (mg/L N)		0.56	0.57	0.51	0.471	0.446	0.434	0.402
Free ammonia as (mg/L N)		0	0	0	0.02	0	0.01	0.04
Total ammonia		0.56	0.57	0.51	0.491	0.446	0.444	0.442
Turbidity (NTU)		0.046	0.045	NA	0.053	0.04	0.043	0.039
Cl ₂ :N Ratio		4.70	4.56	4.86	4.75	4.93	4.82	4.71
LAS+CS	0m	20m	1h	1d	7d	14d	21d	28d
Date	4/11/2018	4/11/2018	4/11/2018	4/12/2018	4/18/2018	4/25/2018	5/2/2018	5/9/2018
Time	15:00	15:20	16:00	15:05	10:51	14:35	8:03	8:24
Location	WCWTP	WCWTP	WCWTP	PP	PP	PP	PP	PP
pH		9.1	9.11	9.13	9.13	9.04	9.04	9.05
Temperature (deg C)		17	17.4	15.3	14.6	15	15.2	15.2
Total Chlorine (mg/L)		2.5	2.51	2.49	2.2	2.19	2.18	2.08
Monochloramine (mg/L N)		0.53	0.54	0.503	0.474	0.447	0.44	0.401
Free ammonia as (mg/L N)		0	0	0.02	0.04	0	0.01	0.05
Total ammonia		0.53	0.54	0.523	0.514	0.447	0.45	0.451
Turbidity (NTU)		0.047	0.047	NA	0.052	0.04	0.045	0.043
Cl ₂ :N Ratio		4.72	4.65	4.76	4.28	4.90	4.84	4.61

Test Results

- Objective 2:** Compare DBP formation for AA/SH and LAS/SH

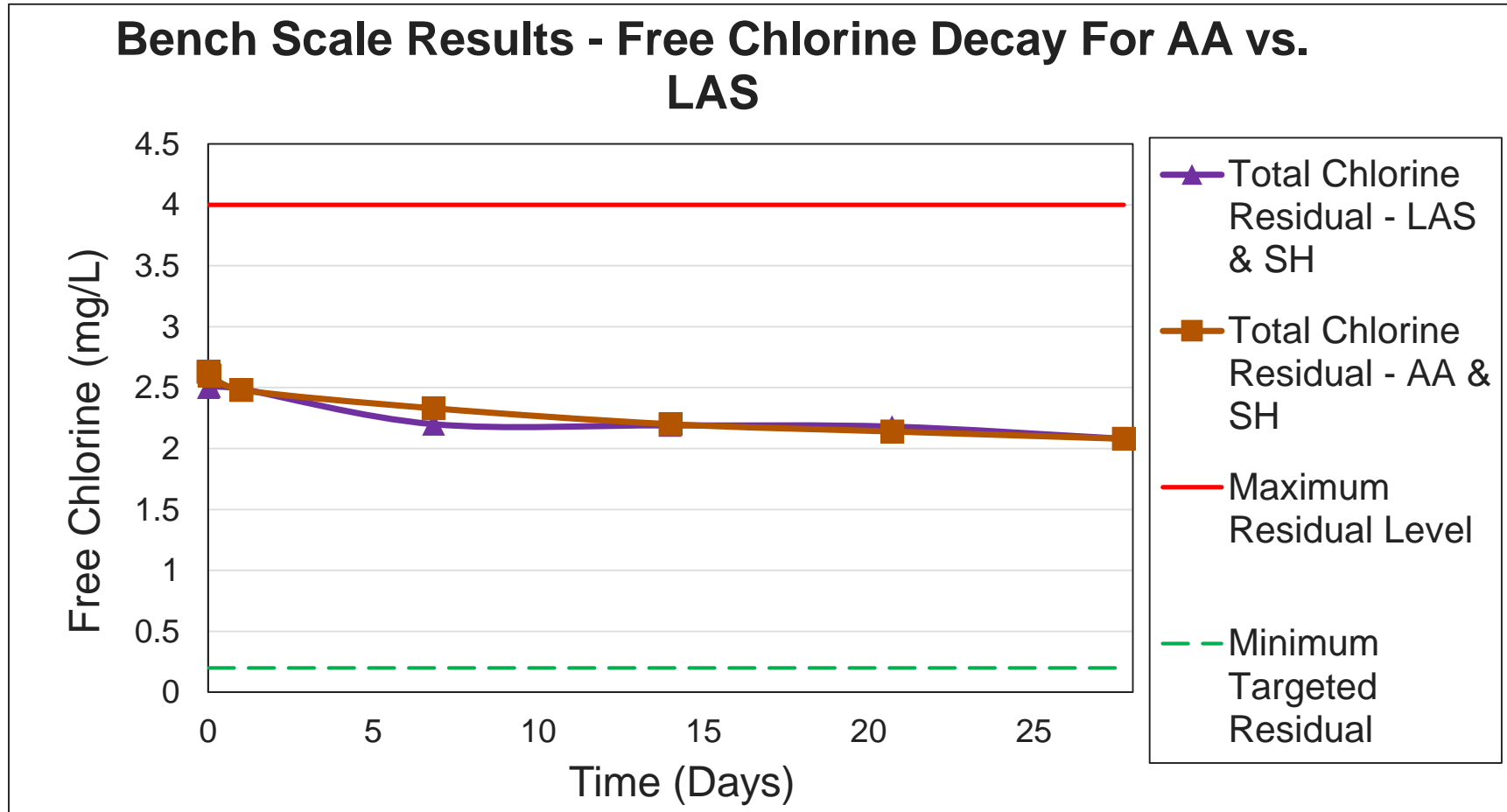
Analysis	Unit	Control Sample	AA &SH 1 Hour Sample	AA &SH 28 Days Sample	LAS &SH 1 Hour Sample	LAS &SH 28 Days Sample	Federal MCL
Testing Date		4/11/2018	4/11/2018	5/9/2018	4/11/2018	5/9/2018	
Total Haloacetic Acids (HAA5)	ug/L	24	23	39	23	38	60
Nitrosamines: N-Nitroso- dimethylamine (NDMA)	ug/L	ND	ND	0.007	ND	0.008	No MCL
Total Trihalomethanes (TTHM)	ug/L	34	28	37	33	36	80

Abbreviation

ND = Nondetectable

Test Results

- **Objective 3:** Compare the rate of chloramine decay when using AA/SH versus LAS/SH



Conclusions

- Chloramination is an effective alternative of chlorination because:
 1. it reduces DBPs formed in drinking water
 2. It maintains a lasting free-chlorine residual in the distribution network
- Chloramination using LAS has no effect on residual decay rates or DBP formation and is safe to store and handle by WTP operators
- EBMUD decided to keep AA systems due to high initial capital cost of replacing current system
- Future studies should be conducted to observe temperature effects of using LAS versus AA for chloramination

References

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Questions?

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